

Fig. 11 - Differences in engine-out hydrocarbon emissions (MMT fuel minus clear fuel) - all cars

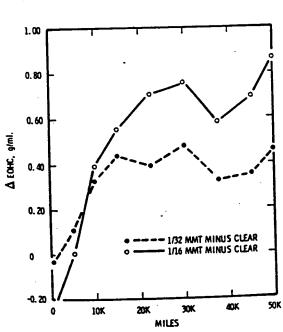


Fig. 12 - Differences in engine-out hydrocarbon emissions (MMT fuel minus clear fuel) - COC cars

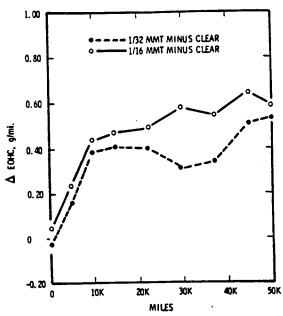


Fig. 13 - Differences in engine-out hydrocarbon emissions (MMT ruel minus clear fuel) - TWC cars

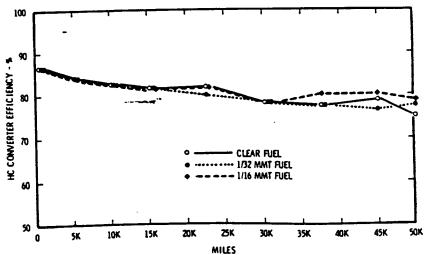


Fig. 14 - Catalytic converter efficiencies for hydrocarbons - average for all cars on each fuel

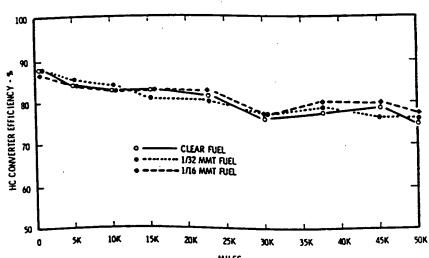


Fig. 15 - Catalytic converter efficiencies for hydrocarbons - average for all COC cars on each fuel

210



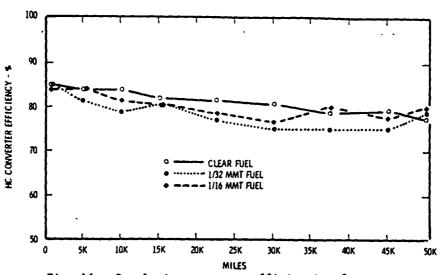


Fig. 16 - Catalytic converter efficiencies for hydrocarbons - average for all TWC cars on each fuel

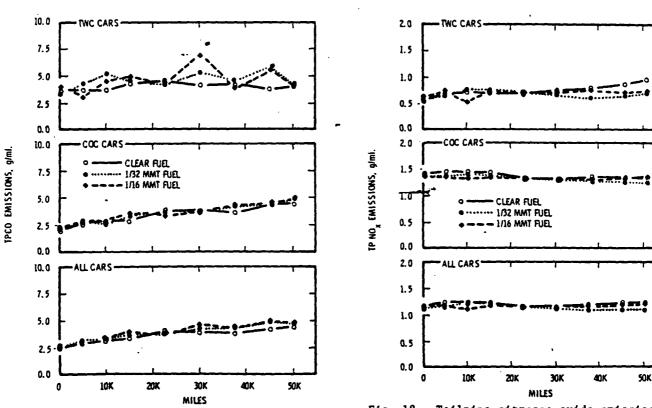


Fig. 17 - Tailpipe carbon monoxide emissions

Fig. 18 - Tailpipe nitrogen oxide emissions



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16 page booklet

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# ATTACHMENT 5

# DETAILED ANALYSIS OF ETHYL TEST DATA

Note: The following figures and tables were derived from the test data which was provided by Ethyl Corporation on floppy disk. No alterations or deletions were made to the as-received data.

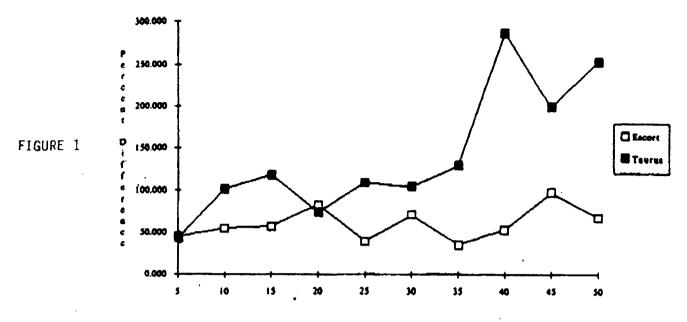
# Percent Effect of MMT over Baseline (Averaged Over Range)

Model	Emissions:	0 - 75	k miles	Emission	s: 0 - 50	k miles
	HC	CO	NOx	HC	ÇO	NOx
С	21.44	8.77	-27.17	23.60	8.44	-22.32
D	5.62	-2.08	7.61	11.05	1.42	12.40
E	8.28	5.07	-7.11	14.04	12.58	-5.33
F	3.01	-34.61	-26.98	0.27	-29.94	-20.44
G	22.67	2.36	-4.69	23.16	-1.26	-1.62
н	5.79	-3.47	-15.75	4.90	-0.65	-7.78
ī	2.57	-7.71	-1.16	-0.05	-9.33	12.52
Т	8.51	-1.34	-28.12	12.41	4.79	-30.54
Ave. %Dif	9.74	-4.13	-12.92	11.17	-1.74	-7.89

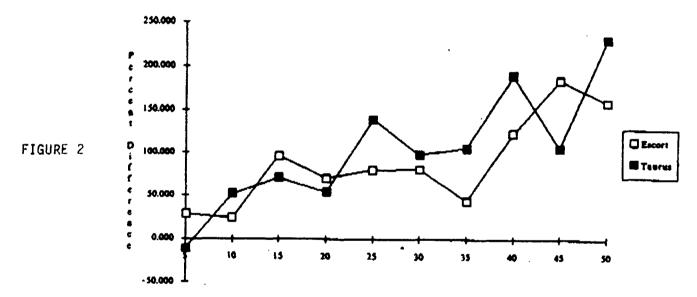
TABLE 1

	Engine Out	:		Tailpipe:		
	MMT	EEE	MMT vs. EEE	MMT	EEE	MMT vs. EEE
50.000 Miles		!				
Escort - HC	1.835	1.790	3%	0.207	0.238	-13%
CO	12.317	12.570	-2%	5.779	6.259	-8%
NOx	2.169	2.145	1%	0.454	0.491	-8%
Taurus - HC	2.889	2.556	13%	0.445	0.419	6%
CO	16.325	16.093	1%	5.986	6.245	-4%
NOx	3.467	3.594	-4%	0.666	0.824	-19%
75,000 Miles						
Escort - HC	1.804	1.651	-9%	0.229	0.238	-4%
CO	11.299	11.841	5%	5.651	6.414	-12%
NOx	2.238	2.266	1%	0.432	0.503	-14%
Taurus - HC	2.802	2.442	-15%	0.415	0.385	8%
CO	14.302	14.160	1%	4.976	5.255	-5%
NOx	4.111	4.287	4%	0.646	0.815	-21%

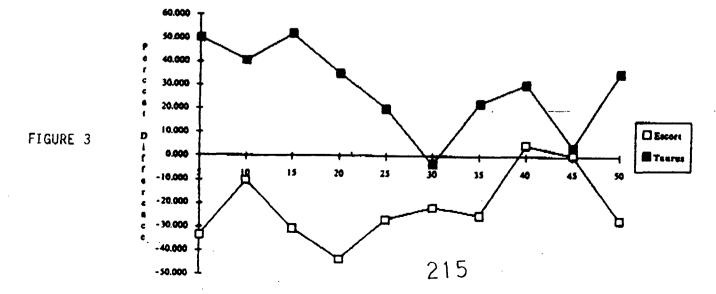
TABLE 2



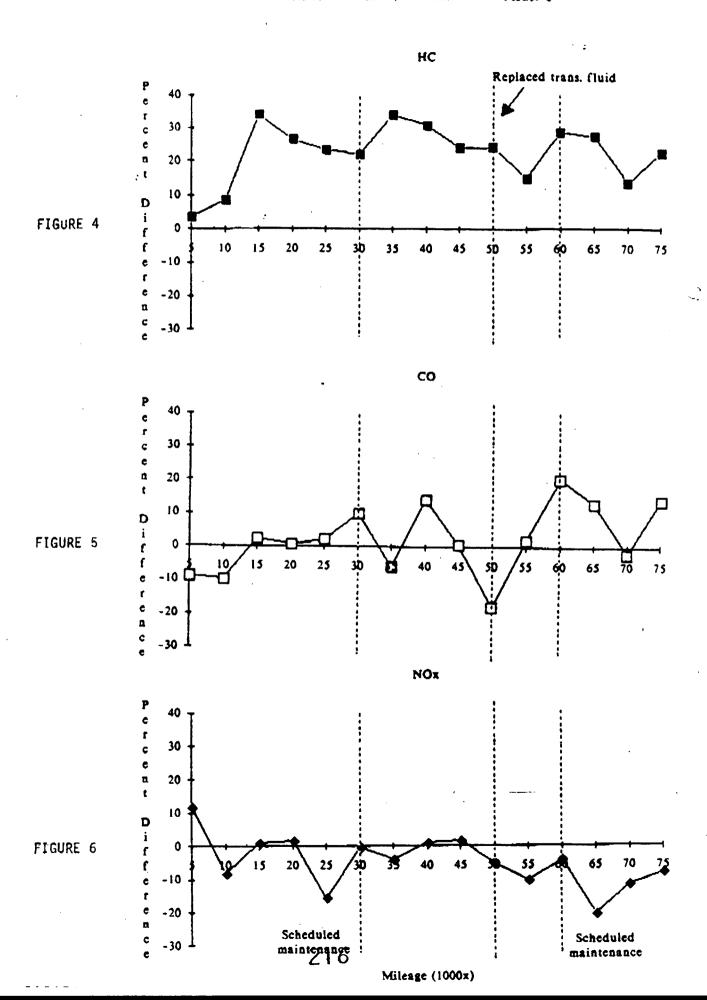
Percent Difference - Ethyl Baseline versus Ford Certification Reissions

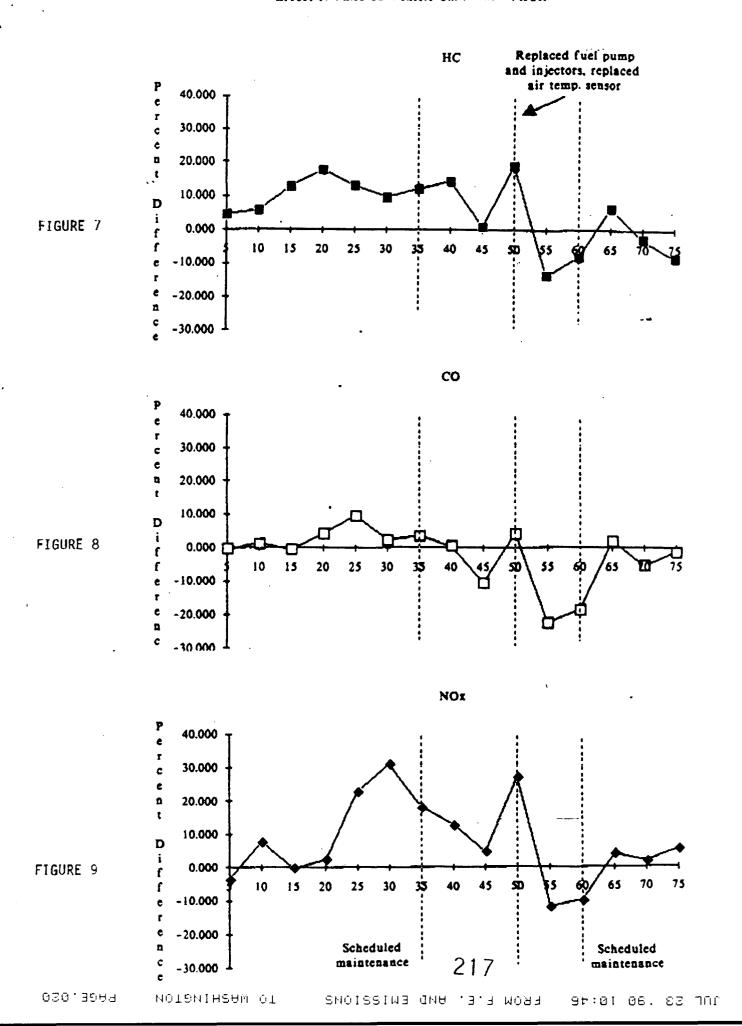


Fercent Difference - Ethyl Baseline versus Ford Certification Emissions

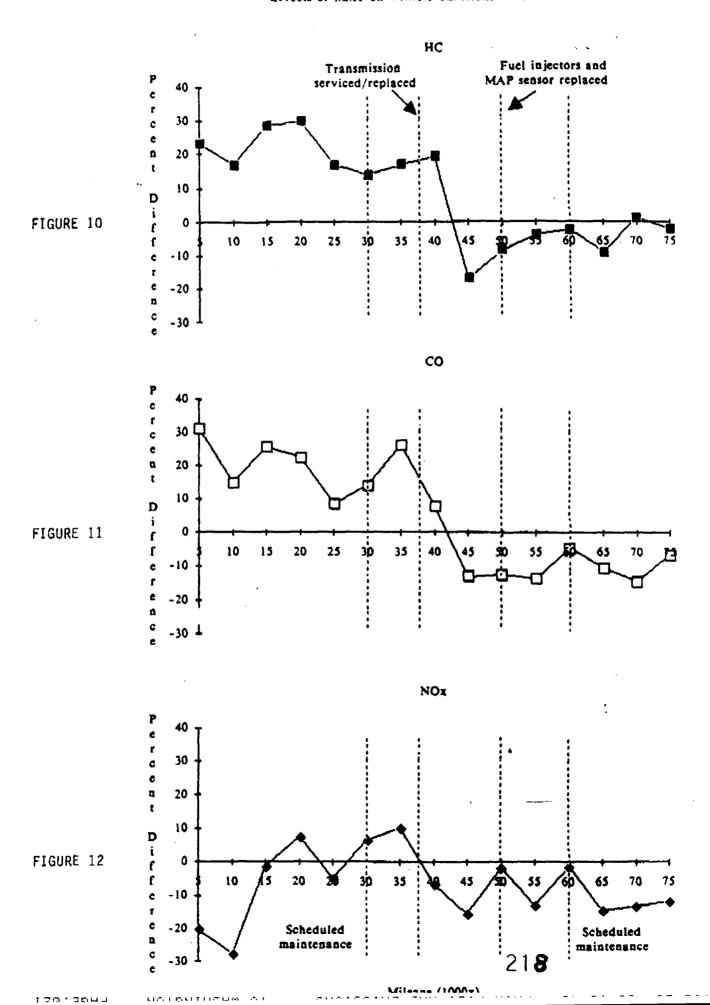


# Effects of MMT on Vehicle Emissions - Model C

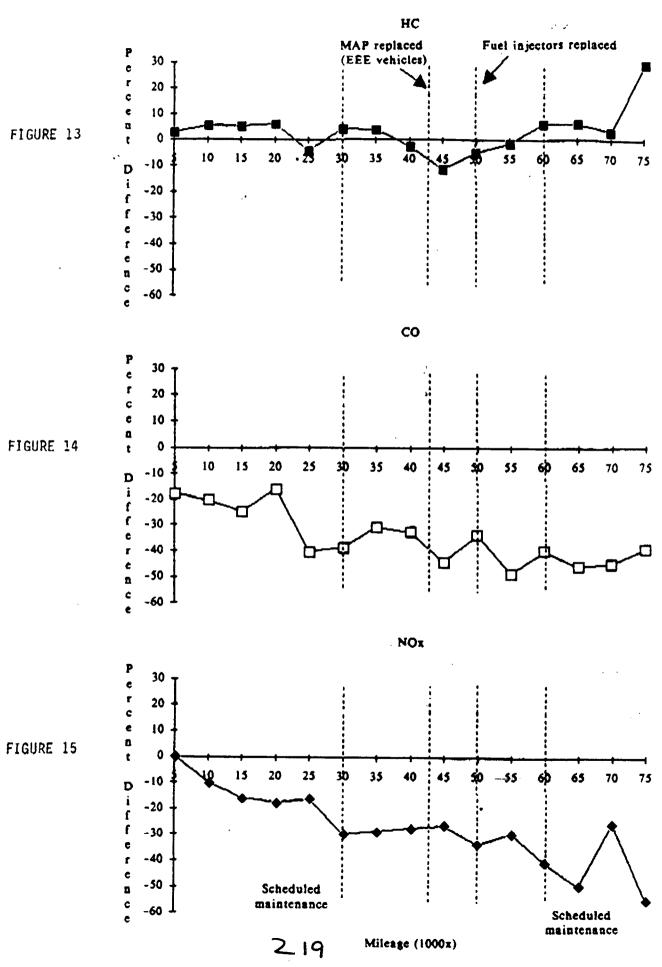




# Effects of MMT on Vehicle Emissions - Model E



# Effects of MMT on Vehicle Emissions - Model F

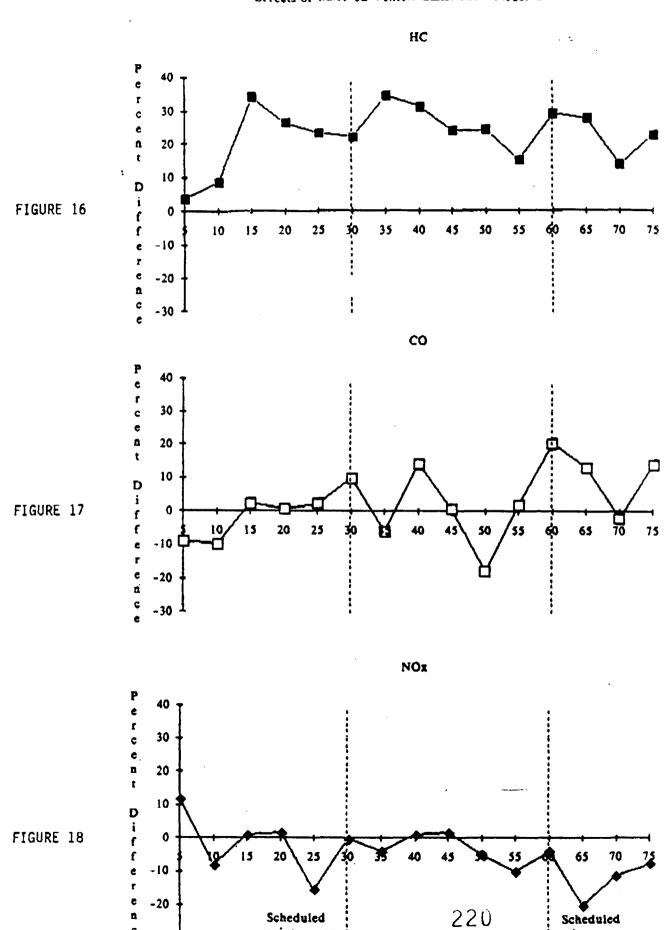


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# Effects of MMT on Vehicle Emissions - Model G



Mileage (1000x)

Scheduled

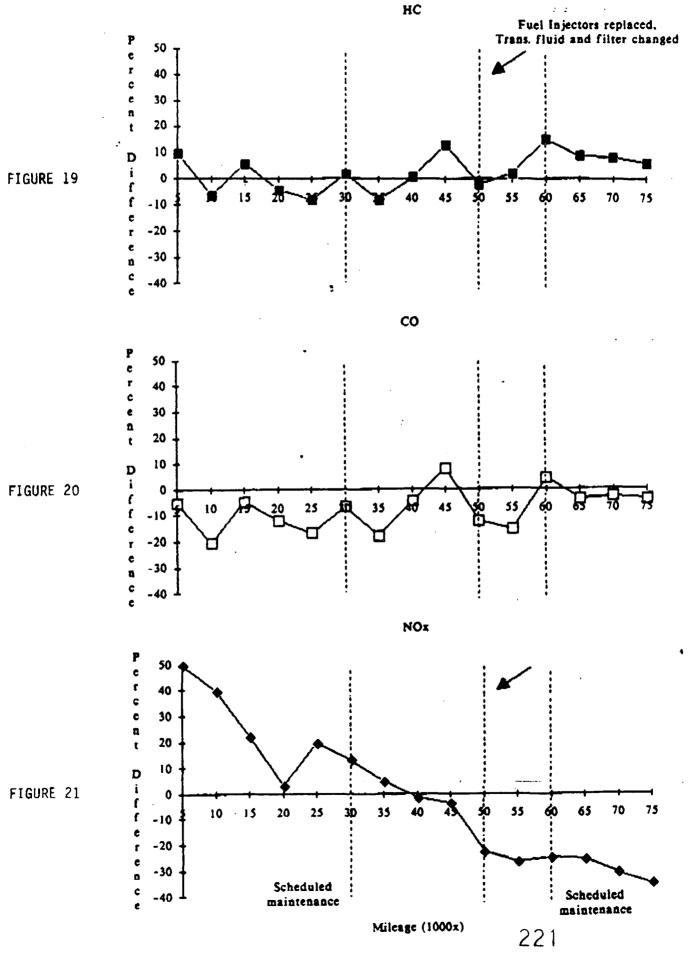
maintenance

Scheduled

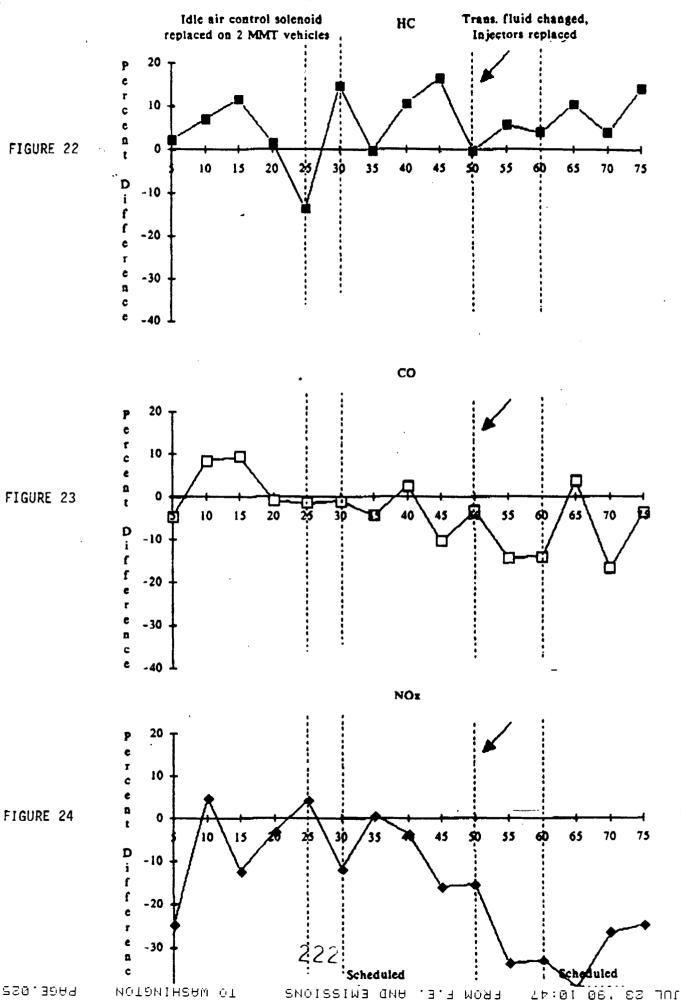
-30

maintenance

# Effects of MMT on Vehicle Emissions - Model H



# Effect of MMT on Vehicle 1



# Effects of MMT on Vehicle Emissions - Model T

HÇ Transmission serviced P Intake air bypass cleaned; 30 (3 MMT & 2 EEE) c Fuel injectors scheduled maintenance r replaced 20 c 10 FIGURE 25 t 0 D 10 15 20 35 45 55 -10 i f f -20 -30 ¢ -40 n -50 CO . . 30

FIGURE 26

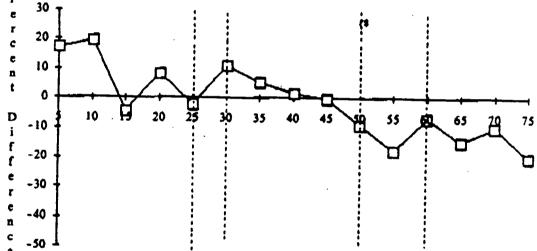
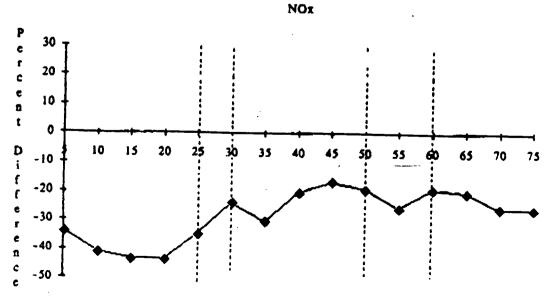


FIGURE 27



Milcage (1000x)



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# Characterization of Automotive Catalysts Exposed to the Fuel Additive MMT

Ronald G. Hurley, William L. H. Watkins

and Robert C. Griffis

Ford Motor Co.

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ISSN 0148 - 7191

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# Characterization of Automotive Catalysts Exposed to the Fuel Additive MMT

Ronald G. Hurley, William L. H. Watkins and Robert C. Griffis

Ford Motor Co.

### **ABSTRACT**

A series of in-use catalysts having mileage of 22,000 to 43,000 miles was characterized to determine the effect of the fuel additive MMT. The analytical techniques included visual examination, x-ray fluorescence, x-ray diffraction, optical microscopy, scanning electron microscopy, and electron microprobe. In addition, catalyst activity was measured and compared to the catalyst activity from a pulsator aged catalyst without the MMT additive in the feed gas composition. Characterization results show a significantly thick layer (5-20 microns) covering the surface of the catalysts which results in the increase of mass transfer resistance. Steady state R and light-off measurements indicated catalyst efficiency is also significantly reduced as exposure to MMT is increased.

In September, 1978 the addition of methylcyclopentadienyl manganese tricarbonyl (MMT) to gasoline fuel was denied by EPA. This denial was based on the failure to establish that the additive MMT would not cause or contribute to the failure of any 1975 or later model year vehicle to comply with applicable emission standards. In the meantime considerable experience has been accumulated in Canada where MMT at a concentration of 16.5 mg/l (1/16 g/gal) is added to fuel as an octane improver. The supplier of the octane improver, MMT, claims to have received no complaints regarding engine or exhaust system performance in approximately 400 billion in-use miles.

Considerable research has been done since the 1978 ruling on the use of MMT as a fuel additive (1-5). Wallace, et al. (5) and Benson, et al. (1) have shown that with 88% to

99% confidence that MMT adversely affects light duty vehicle tail pipe HC emissions at the MMT concentration 16.5mg/gal. Conversely, MMT did not statistically show a consistent adverse effect on CO or  $NO_X$  exhaust emission. Hughmark, et al. (4) conclude that MMT actually increases converter efficiency in relation to clear fuel. Williamson, et al. (2) concluded that the "catalyst enhancement phenomena" which resulted in the 2-3% HC improvement in catalyst efficiencies in the CRC study as well as the apparent beneficial effects observed in his research can perhaps be attributed to the scavenging effect or to catalytic activity of the MMT combustion product, Mn<sub>3</sub>O<sub>4</sub>(3). However, in each case the author examined the effects of MMT on emissions and did not particularly focus on the effects on the catalyst or determine the possible mechanism of catalyst deactivation. Consequently, and in response to the possibility of the EPA granting a waiver of the 1978 ruling and the subsequent use of an MMT additive in US gasoline, a study was undertaken to characterize, examine and evaluate a series of catalysts removed from in-use vehicles. The major objective of this paper, therefore, is to present an evaluation and characterization of the long term durability and efficiency of catalysts exposed to the fuel additive MMT.

### **EXPERIMENTAL**

Nine (9) catalysts (Table 1) that had been exposed to MMT were removed from vehicles under warranty because of suspected converter defects. It should also be noted that these catalysts were taken from vehicles in which the authors had no means of verifying their fueling characteristics nor their proper function. Therefore, it was assumed by the authors that the vehicles used for this study were properly adjusted and fueled with gasoline that met the Canadian standard of 1/16 g/gal of MMT. As shown in Table 1 some of these converters were

a two brick system and others were a single brick system. On the average these vehicles had accumulated 30,000 in-use miles. Characterizations performed consisted of visual examination, analysis by x-ray fluorescence (XRF), BET surface measurements, optical and scanning electron microscopic (SEM) examination of the washcoat conditions, contamination profiles and catalyst activity. Each of these analytical techniques is a standard post-mortem method for the characterization of in-use catalysts and will not be described in this paper.

Table 1

Vehicle Aged Catalysts Evaluated for Effects of MMT

Engine		Model	Vehicle	<b>:</b>	
<u>No.</u>	<u>Type</u>	<u>Year</u>	<u>Type</u>	<u>Miles</u>	<u>Bricks</u>
301-A	2.8L	1984	Bronco	II 43K	2
301-B	2.3L HSC	1986	Topaz	24K	2
301-C	2.3L HSC	1985	Tempo	34K	1
301-D	1.9L 2V	1986	Lynx	22K	2
301-E	1.9L 2V	1985	Escort	28K	2
301-F	2.3L HSC	1984	Topaz	28K	1
301-G	2.3L HSC	1986	Тепро	22K	1
301-H	2.3L EFI	1985	Merkur	32K	2
301-I	2.3L OHC	1984	Ranger	33K	2

The catalysts received for evaluation, as shown in Table 1, were from 1984-1986 vehicles equipped with either 2.3L, 2.8L, or 1.9% engine. Each catalyst was sampled using standard techniques that have been described elsewhere in the literature (2). For x-ray fluorescence (XRF) the catalyst was cored and the resulting core divided into samples of inlet, middle, and outlet for amadysis. Each sample consisted of approximately 6 grass of catalyst or sample plus corderite (fresh substrate) to approximate 6 grams. From a core portioned inlet, middle, and outlet a 0.5 gram sample from each was used for the standard BET analysis. Optical and scanning electron microscopic (SEM) samples were also selected in a similar manner as the XRF samples. For this analysis each inlet, middle and outlet sample was mounted and polished to provide a flat surface for analysis. Additional SEM samples were taken by breaking off portions of the catalyst, coating with a thin lawer of gold or carbon to provide a conductive swrface, and mounting on a carbon block for swrface morphological examination. Samples for datalyst activity, steady state R and light-off analysis contained only the first 1/2 inch segment of inlet, middle, and outlet. Instrumentation for the MMT characterization included a SIEMENS SRS 300/VAX x-ray fluorescence spectrometer for XRF analysis. A QuantChrom Quantector Gas Flow System with a Quantasorb Flow Comtrol Accessory was used for BET surface area measurements. The scanning electron microscope used in this

characterization was an ETEC Autoscan equipped with a DELTA 3 Kevex energy dispersive x-ray system and a Kevex QUANTUM detector. Optical micrographs were taken using a Reichert metallograph for macros and a Neophote metallographs for micros. Steady state three-way activities and light-off curves were measured in a flow reactor over a range (lean-to-rich) of feed gas compositions.

#### RESULTS AND DISCUSSIONS

The typical as-received condition of the catalysts used in this study is shown in figure 1. Visually, the interior of the converters have a heavy to moderate coating of a rust colored residual deposit. Further visual inspection show that all of the catalyst cores have light to moderately heavy channel clogging of the inlet core of the first brick. Channel clogging of the catalyst core appears to be consistent and is limited to the first brick of the converter. Only one of the converters shows visual signs of exposure to high operating temperatures. This converter is shown in figure 2.

The results of x-ray fluorescence analysis of samples taken from each catalyst are shown in Table 2. These results summarize the concentration of the contaminants found to be present on the catalysts examined. Manganese concentration, as one might expect, is highest on the inlet of the catalyst and decreases toward the outlet. The Mn concentration range on the first brick, between a low of 1.4 wt% for a vehicle mileage of 24,000 to a high of 6.4 wt% for a vehicle having accumulated 33,000 in-use miles. The x-ray data are consistent with the visual examination in that the highest Mn concentration is limited to the first brick of the converter. The anomaly of Mn concentration reversal (low Mn on the inlet and higher on the outlet) as shown in 301D-1,-2 is due to exposure of this catalyst to high operating temperature which resulted in substantial substrate melting (figure 2). It is important to note that other contaminants S, P, Zn, and Pb, are generally in an acceptable range, somewhat higher than one might expect for this level of accumulated mileage. In addition, one might also expect that the Pb concentration would be higher than normal because of the possibility of the use of fuel from lower quality fuel refineries. This is evident in some of the catalyst but not to an extreme degree. The x-ray results are inconclusive in their tendency to confirm earlier studies that Mn<sub>3</sub>0<sub>4</sub> acts as a scavenger (3) in the exhaust for transporting away fueland oil-derived catalyst poisons such as Pb, P, and Zn.

X-Ray diffraction analysis of the finely divided, rust colored deposits on the first brick indicates that this residual layer is primarily  $\rm Mn_3O_4$ . These results confirm earlier experimental results (3,5) in that Mn derived

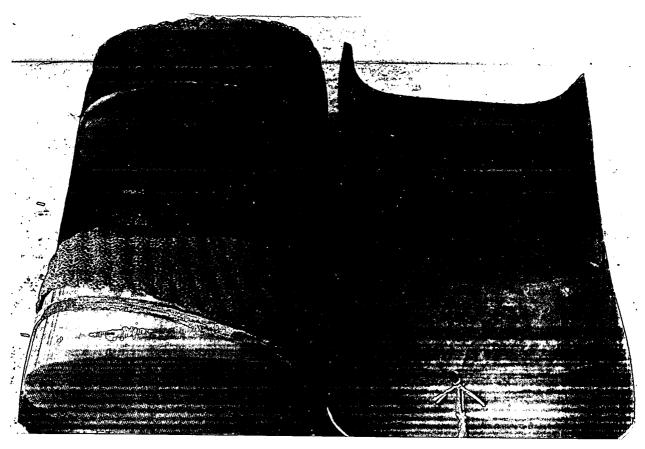


Figure 1. Example of the as-received condition of the in-use converters.

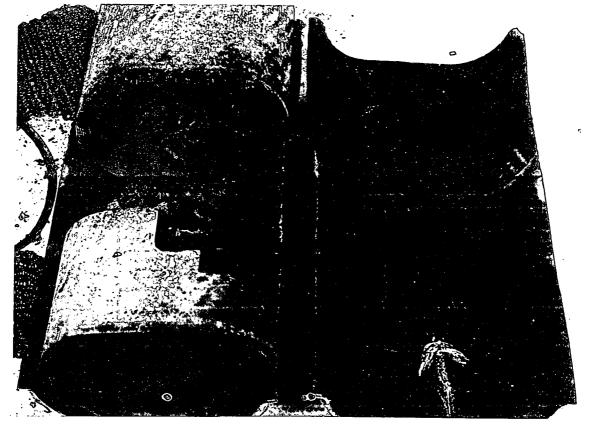


Figure 2. Example of in-use converter showing exposure to high operating temperature in the as-received condition.

Table 2
CONTAMINANT ANALYSIS OF AUTOMOTIVE CATALYSTS EXPOSED TO MMT

Vehicle				Contam	inants. Wt%	<del></del>	
<u>Catalyst</u>	Miles	<u>Type</u>	Mn	S	P	Zn	Pb
301A-1 I	43,000	TWC	2.08	0.0	.46	.14	.67
M	•		.83	0.0	.16	.05	.04
0			.53	0.0	.10	.03	.07
301A-2 I		COC	. 83	0.0	.16	.06	.21
M			.28	0.0	.06	.02	.12
0			. 26	0.0	.05	.01	.12
301B-1 I	24,000	TWC	1.43	.14	.13	.12	.07
M 0			.37 .35	.12 .12	.06 .06	.03 .02	.03 .06
						•	
301B-2 I		coc	. 48	.21	.08	. 02	.04
M O			.19 .16	. 20 . 16	. 04 . 04	.01 .01	.02 .01
					.04		.01
301C I	34,000	TWC	5.20	.14	. 39	.28	.41
3010 1 M	34,000	140	2.57	.05	. 25	.13	.22
0			2.24	.03	. 23	.10	. 21
301D-1 I	22,000	TWC	. 79	.0	.07	.02	.03
М			.80	.0	.06	.01	.02
0			2.18	.01	.18	.09	.19
301D-2 I		COC	1.62	.16	.11	.01	.07
M			.69	.02	.06	.01	.23
0			.60	. 06	.06	.02	.13
301E-1 I	28,000	TWC	1.77	.05	.18	.08	.54
М			.91	.05	.09	.02	.02
0			1.08	.08	.09	.02	.02
301E-2 I		COC	1.76	.12	.13	.04	. 30
M O			. 86 . 77	.10 .11	. 08 . 07	.01 .01	. 34 . 49
			.// 	. <u></u> .	.07	.01	.49
301F I	28,000	TWC	3.15	.11	. 22	. 20	. 74
M M	20,000	1#0	2.14	.06	.11	.11	.46
О			1.76	.05	.10	.08	. 37
301G I	22,000	TWC	4.20	. 26	. 27	. 24	. 22
М			2.05	.11	.19	.13	.09
0			1.58	. 14	.15	. 09	.06
20111 1 7	22 000	TT 1C					
301H-1 I M	32,000	TWC	1.72 .92	.12 .13	. 24 . 12	. 25 . 11	.02 .03
0			.75	.12	.10	.07	.03
301H-2 I		coc	.81	.12	.11	.08	. 04
M		000	.51	.13	.06	.04	.03
. О			.41	.14	.06	.03	.03
301I-1 I	33,000	TWC	6.14	.02	.63	5.8	. 52
M			2.70	.0	. 29	. 13	. 14
0			1.98	.0	. 25	. 11	.08
301I-2 I		COC	3.39	. 0	. 37	. 28	. 33
М О			1.71 1.49	.0	.18	.06	. 09
U			1.47	. 0	. 16	. 04	.11

from MMT is converted in the combustion process exclusively to  $Mn_3O_4$ .

Optical micrographs (figures 3 and 4) of catalysts, 301G and 301I, show a heavy residual layer covering the washcoat. X-Ray fluorescence results indicate that these two samples, contain approximately 4 and 6 wt% of Mn, respectively and are from vehicles with 22,000 and 33,000 accumulated in-use miles. As is evident in both of the high magnification micrographs, from 301G and 301I, the Mn<sub>3</sub>O<sub>4</sub> is on layered on the surface of the washcoat. It does not appear to penetrate or have reacted with the washcoat but simply adheres to the surface. This deposit of Mn<sub>3</sub>O<sub>4</sub> on the washcoat may cause physical pore plugging and thus result in mass-transfer problems.

Scanning Electron Microscopic and Electron Probe analysis show the thickness of the Mn<sub>3</sub>0<sub>4</sub> residual layer to range from approximately 5 microns to a maximum of approximately 20 microns. The thickest layer is observed on catalyst 301I which had 33,000 accumulated miles. SEM micrographs (figure 5) of crosssections of 301G and 301I show this layer quite distinctly. Also shown in this figure is a Mn x-ray elemental map pattern to confirm that the layer is indeed rich in Mn. This elemental map is used to determine the actual thickness of the Mn rich region on the washcoat. This micrographs also indicate little if any penetration into the washcoat by the Mn rich layer. Indications from the surface morphology study is that the Mn rich layer does simply adhere to the surface of the washcoat. An example of the surface morphology of the Mn rich layer is shown in figure 6. As is shown in the micrograph the surface is covered with a layer of fluffy, porous material. This material was confirmed by XRD to consist exclusively of Mn304.

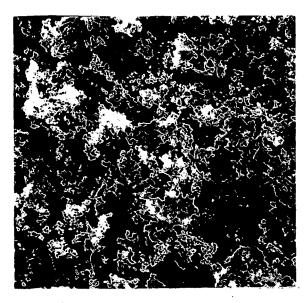


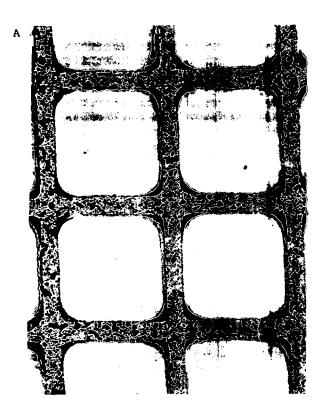
Figure 6. Surface morphology of Mn rich layer on 33,000 mile MMT exposed catalyst.

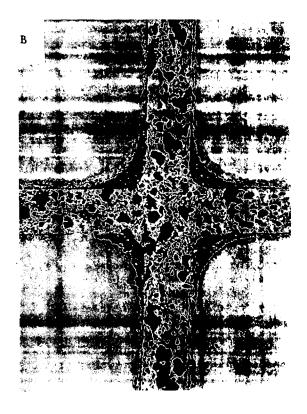
BET surface areas (Table 3) range between  $14.0 \text{ m}^2/\text{gm}$  and  $0.9 \text{ m}^2/\text{gm}$  for the first brick and between  $9.3 \text{ m}^2/\text{gm}$  and  $0.6 \text{ m}^2/\text{gm}$  for the second brick. In general, as shown in Table 3, all the surface area measurements were lower than that of a fresh catalyst's surface area of approximately 25 m<sup>2</sup>/gm. The lower BET values measured for the catalysts could be due to two mechanisms: 1) exposure to higher than normal operational temperatures and 2) the reduction of active surface area sites by the heavy coating of Mn<sub>3</sub>O<sub>4</sub>. However, there is no prior experimental evidence that the combustion products of MMT reduces "active surface area sites". Most likely the Mn<sub>3</sub>O<sub>4</sub> deposits cause pore plugging and subsequent mass transfer problems. This diffusion hinderance would certainly be reflected in a erroneous decrease . of the BET areas, if measured by one-point dynamic desorption.

Conversion efficiencies were measured for two of the MMT exposed catalysts, 301G and 301I having accumulated 22,000 and 33,000 miles, respectively. In addition, a comparison of the catalyst efficiency was made between a pulsator aged catalyst and the MMT exposed catalysts. The pulsator aged catalyst was aged with a "low-lead" (no MMT) simulated certification fuel, i.e., isooctane containing 2 mg Pb + 0.8 mg P + 0.03 wt % S/gal, to the equivalent of 15,000 miles. The activity and three-way selectivity of catalysts is expressed as percent conversion of NO, CO, and HC against the redox ratio (R) of the reacting gas mixture. These points are plotted over a range of rich to lean air fuel ratio to obtain an R curve. Optimum selectivity and redox ratio values corresponding to the peak three-way conversion point are determined by interpolation from resulting curves. As shown in equation below, R is obtained by dividing the sum of the equivalent reducing components of the mixture by the sum of the oxidizing components. Thus

$$R = \frac{pCO + pH_2 + 3nC_nH_2n + 3.33npC_nH_2n + 2}{pNO + 2pO_2}$$

Therefore a value of R > 1 represents an overall reducing gas mixture and a value of R = 1 represents a stoichiometric gas mixture. The redox ratio, a measure of the exhaust stoichiometry and related to the A/F ratio, is a measure of the fuel mixture stoichiometry. It is a more sensitive yardstick, since, in the exhaust, most of the mixture has been burned away. Steady-state R curves (measure of catalyst conversion efficiency with respect to HC, NO, and CO) and light-off temperatures were measured on a flow reactor over a range (leanto-rich) of feed gas composition. A comparison of steady-state R curve data (figure 7) between the MMT exposed and a non-MMT exposed catalyst indicate equal deterioration among the three catalysts for CO activity. However, there was





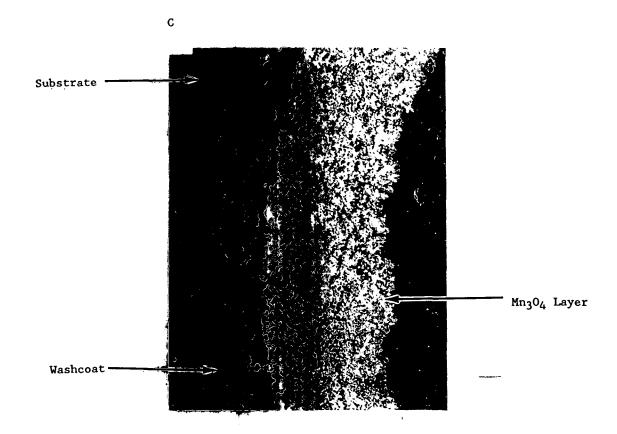
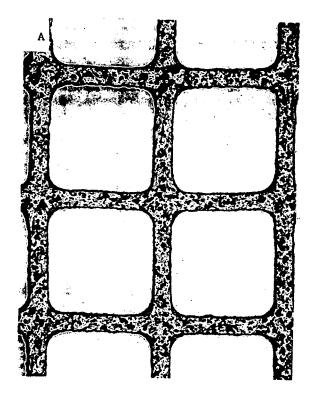
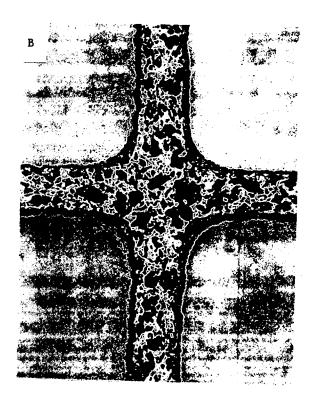


Figure 3. Optical Micrographs of 33,000 mile MMT exposed catalyst TC-301I at (a) 30X, (b) 80X, and (c) 800X.





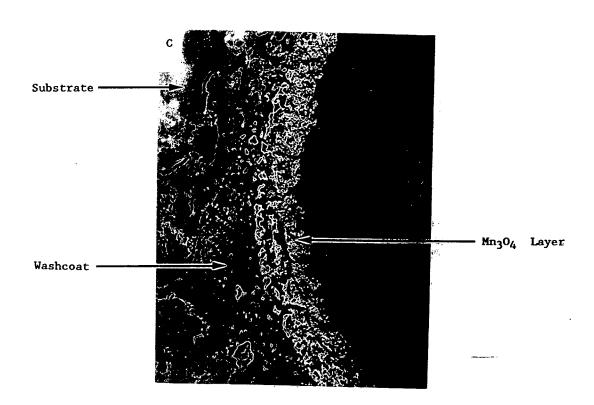
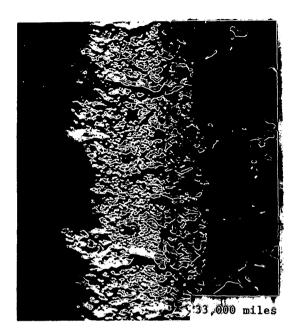
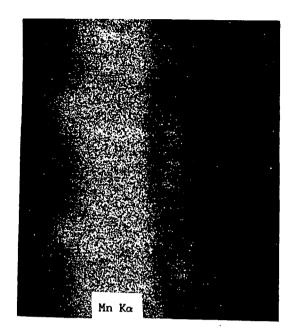
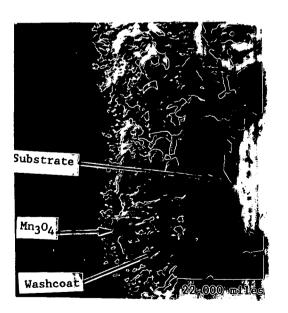


Figure 4. Optical micrographs of 22,000 mile MMT exposed catalyst TC-301G at (a) 30X, (b) 80X, and (c) 800X.







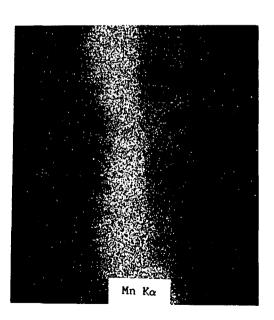


Figure 5. Scanning electron micrographs and Mn K $\alpha$  elemental maps of (a) 33,000 miles MMT exposed catalyst and (b) 22,000 miles MMT exposed catalyst. (1 cm = 10 microns).

В

A

Table 3

B.E.T. SURFACE AREA MEASUREMENT OF AUTOMOTIVE CATALYSTS EXPOSED TO MMT

B.E.T.	SURFACE AR	<u>EA MEASUREMENT OF</u>	AUTOMOTIVE	CATALYSTS	
<u>Vehicle Ca</u>	<u>talysts</u>	<u>Type</u>	Miles		B.E.T. <u>Area (M<sup>2</sup>/g)</u>
301A-1	I	TWC	43,000		3.8
	M				6.8
	0				4.5
301A-2	I	COC			2.7
	M O				4.1 4.0
					4.0
301B-1	I	TWC	24,000		13.9
	M				15.4
	0				12.8
301B-2	I	COC			7.6
	M O				8.7 8.2
				· ·	
301C	I	TWC	34,000		8.5
3010	M	25	3.,500		7.4
	0				7.0
301D-1	I	TWC	22,000		. 8
	M O				.5 1.3
301D-2	I	сос			.3
J01D-2	M	000		•	. 3 . 7
	0				4.0
2015 1		TILO	00 000		, ,
301E-1	I M	TWC	28,000		4.4 5.6
	0				5.5
301E-2	I	coc			6.9
	M		•		7.9
	0				8.6
	_				4
301F	I M	TWC	28,000		14.1 12.4
	0				11.0
301G	I	TWC	22,000		7.3
	M		·		6.7
	0				6.6
301H-1	I	TWC	32,000		8.9
	M		•		9.8
	0				9.8
301H-2	<b>I</b> .	COC			8.4
	M O				10.2 9.3
3011-1	I	TWC	33,000	•	3.8
	M	<b>-</b>	<b>,</b>		4.0
	0				4.3
3011-2	I	COC			1.2
	M O				0.4
	5				0.5

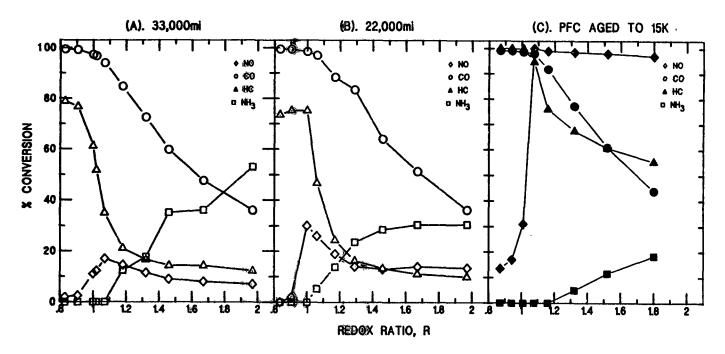


Figure 7. Comparison of the steady-state NO, CO, and HC activities for (a) 33,000 miles MMT exposed catalyst, (b) 22,000 miles MMT exposed catalyst, and (c) 15,000 mile non-MMT pulsator aged catalyst.

extreme deterioration of NO and HC activity for the MMT exposed catalysts. The peak NO conversion as measured at an R value of 1.07 was 100%, 27%, and 15% for the pulsator aged catalyst and the MMT catalysts 301G, 301I, respectively. The peak HC conversion at an R value of 1.07 was measured to be 95%, 43%, and 32% for the pulsator aged catalyst and the MMT catalysts 301G, 301I, respectively. In addition, the data indicate that NH3 formation increases as the catalyst is exposed to MMT. This is understandable because Mm304 is not a selective catalyst to reduce NO to N2.

A comparison of steady-state light-off curve data (figure 8) between the MMT exposed and a non-MMT exposed catalyst show 80% conversion for HC, CO, and NO for the palsator (non-MMT) catalyst to be at approximately 280° C. Whereas 80% conversion for CO was approximately 410° C for catalyst 301G and approximately 460° C for catalyst 3011. Eighty (80) percent conversion does not take place for HC or NO for either MMT exposed catalyst. The curves also show that 50% conversion of HC, CO, and NO takes place at approximately 2500 C for the pulsator aged catalyst. Fifty (50) percent conversion for CO and HC takes place at 350° C and 460° C, respectively, for catalyst 301G. Likewise, 50% conversion of CO and HC takes place at  $400^{\circ}$  C and  $530^{\circ}$  C, respectively, for catalyst 3011. The data indicate that 50% conversion does not take place for NO on either of the MMT exposed catalyst.

## CONCLUSIONS

Although the authors had no means of verifying the fueling characteristics of the vehicles nor the proper function of the vehicles from which the catalysts were taken, the conclusions are based on the assumption that these vehicles were properly adjusted and fueled with gasoline containing 1/16 g/gal MMT. The following salient results obtained from the post-mortem analysis of these catalysts can be summarized as follows:

- Minor to severe clogging of the first brick by the residue of the oxidation product of MMT, Mn<sub>3</sub>O<sub>4</sub>,
- 5-20 micron thick layer of Mn<sub>3</sub>O<sub>4</sub> over the washcoat surface,
- decrease in surface area (BET) measurements.
- percent conversion of NO, CO, and HC decreases as the exposure to MMT increases,
- NH<sub>3</sub> formation increases as the exposure to MMT increases;—and,
- light-off temperatures for NO, CO, and HC increase as the exposure to MMT increases.

The mechanism of deactivation as determined by this analysis is due to the clogging of the

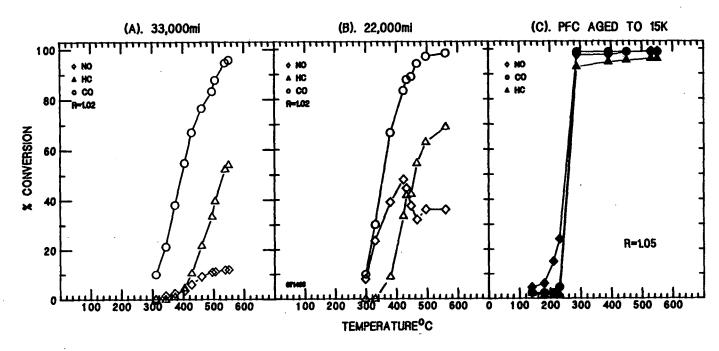


Figure 8. Comparison of the light-off NO, CO, and HC activities for (a) 33,000 miles MMT exposed catalyst, (b) 22,000 miles MMT exposed catalyst, and (c) 15,000 mile non-MMT pulsator aged catalyst.

channels of the converter. This plugging of the channels of the monolith results in an increase of the mass transfer resistance and consequently reduces the efficiency of the catalyst to convert HC, CO and NO<sub>X</sub>. Based on these results it appears that the fuel additive MMT had a deleterious effect on the efficiency of the catalysts tested. However, in order to access more definitively the effect of MMT on in-use vehicle catalyst efficiency, this study suggests the need to correlate cause and effect from vehicles fueled with and without the fuel additive MMT.

### **ACKNOWLEDGEMENTS**

The authors gratefully acknowledge F. A. Alberts, W. Allie, Jr., R. K. Belitz, F. W. Kunz, and C. R. Peters who performed the many analytical analyses required by this characterization. The authors also acknowledge the helpful assistance of personnel from the Fleet Test Section, G. Bourdage, R. McCasland, L. Shannon, and D. Taylor and from Ford Canada Parts and Service, D. McIntosh and R. McTaggart. In addition, the authors acknowledge J. G. Thom and H. S. Gandhi who provided helpful criticism of the paper.

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